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# NOVEL PULSATILE CARDIAC ASSIST PUMP

by

# LAKSHMI MOHANADAS

# THESIS

Submitted to the Graduate School

of Wayne State University,

Detroit, Michigan

in partial fulfillment of the requirements

for the degree of

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Approved By:

Advisor

Date



# **DEDICATION**

То

My Parents and friends



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#### CHAPTER 1

# **INTRODUCTION**

Cardiac pumps are revolutionary devices which assist the failing heart function. Over the decade many cardiovascular pumps have been developed to assist the heart. These devices are generally mechanical pumps which help in efficient blood circulation. Due to the increase of cardiac complications after a surgery and the number of patients suffering from heart functioning problems, the demand of heart assistive pumps has also increased in the market which can efficiently increase the heart functioning rate and there by enhance the patient's condition. There are two types of patients who generally need the use of a pump to support the function of their heart. One, those who need immediate assistance after an heart attack or a heart surgery and two, those who are waiting for a heart transplant and they have long wait time. This wait time till transplantation is called as bridge to transplantation. Sometimes these pumps are also used as end therapy, that is the pump is used to provide good quality of life till the recovery of the patient and no transplantation occurs. This usage is also known as bridge to recovery.

In general, the blood pumps are classified on the basis of their mechanical action. The two such categories are: displacement pump and rotary pump [1]. Displacement pumps work on the basis of energy transfer due to periodic changes whereas a rotary pump changes the velocity of the impeller vanes. Rotary pumps become more advantageous over displacement pumps when large volume flow at low pressure is required. But when the low volumetric flow is required with high pressure, displacement pumps are preferred. Displacement pumps are vastly used in the medical field over the past decades for



cardiopulmonary bypass in heart lung machines and in the dialysis machines. These pumps have been widely in use due to their simplicity and low cost. But the major disadvantage caused by them is blood damage and particulate spallation.

On the contrary rotary pumps are more advantageous over the displacement pumps as they possess less blood damage, smaller in size, better transportability, and absence of spallation. Due to all these advantages over displacement pumps, centrifugal pumps, a type of rotary pump, is gaining lot of market in the cardiopulmonary bypass application. But due to the use of rollers, these can be used upto a time limit of 4 hours as there is risk of blood cell damage and to compensate high doses of anticoagulation drugs are also used. These are used to assist patients after an open heart surgery who suffers from low cardiac output known as low output syndrome (LOS) but fails to do so. Hence in treatment more of inotropic and vasoactive drugs are used.

A number of different types of rotary and displacement pumps are still used as ventricular support system. Micro-axial pump is one such type from rotary pumps group which are introduce through femoral artery and its inflow cannula is place through the aortic valve to the left ventricle. The first axial-type blood pump was introduced into the market by Johnson & Johnson (Division of Ethicon Inc., Arlington, TX, USA) under the name of 'Hemopump'[1].

Another type is the pneumatic displacement pump which is introduced through thoracotomy. These pumps possess the risk of skin infection at their penetration sites. Also the patient has less mobility due to the bulkiness and the moving consoles. To compensate old mechanical support systems, fully implantable electro-mechanical left ventricular assist devices (LVADs) have been developed. Two such systems that are



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currently available are the NOVACOR (Baxter Healthcare Corp., Deerfield, IL, USA)[3][4] and the HeartMate (Thermo Cardiosystems Inc., Woburn, MA, USA)[5].

Rotary pumps are classified generally into three categories according to the impeller geometry: Radial (centrifugal), axial and diagonal. Axial flow pumps are efficient at low pressure differences and generate high volumetric flow whereas a radial pump is designed to produce low flow rates at high pressure. Diagonal pumps also known as mixed flow systems, generally operate at high pressure to provide high flow rate.

As stated rotary pumps have a number of theoretical and practical advantages over the displacement types. They have low blood trauma, lesser anti coagulation levels and therefore lesser chances of hemorrhage. Also depending on the design, they can also be coated with heparin. A detailed tree chart description of different types of pumps available in the market is provided in figure 1 and figure 2 [1]. A further more detailed description of the devices in the market is given in tables 1,2,3 and 4. These tables shows the description of the pumps mentioned in the figure 1 and 2. The pump name and the company which prototyped it along with the application, the position of the pump, what type of support does the pump offer and for what duration the pump is used is provided in the table. Table 2 specifically enumerates the different types of centrifugal pumps in the market with their developers and the duration for which they are used.





Fig 1: Type of Blood pumps [1]



ROTARY BLOOD PUMPS									
Axial F	Pumps	Radial	Pumps	Diagonal Pumps					
Hemopump	Jarvik 2000	Biopump	Capiox SP	VentrAssist	Heart Quest				
Sun Waseda (IVAP)	DeBakey	Delphin	Isoflow (Lifestream)	Delta Stream	HIA Micro Diagonal				
HeartMate II	Impella	Rotodynamic Pump	Gyro Pump						
Valvo Pump	Streamliner	Rota Flow	HiFlow						
		Nikkisso Pump	AB-180						
		Vienna Centrifugal	Evaheart						
		Abiomed CF	Kriton Pump						
			Heart Mate III						

Fig 2: Types of Rotary Pumps in the market



Pump	Organization	Application	Position	Support	Duration
Hemopump	Medtronic Inc., Minneapolis, MN, USA	Postcardiotomy/ coronary surgery	Implantable intra-arterial/ transvalvular (aortic valve)	Left ventricular	Short term/ medium term
Jarvik 2000	Jarvik Heart Inc., Oxford Heart Centre, USA/UK	VAD/BTT	Implantable intraventricular	Left ventricular	Long term
IVAP	Sun Medical Co., Waseda University, Tokyo, Japan	VAD/BTT	Implantable intraventricular	Left ventricular	Long term
DeBakey VAD	MicroMed Technology Inc., Texas, USA	VAD/BTT	Fully implantable abdominal	Left ventricular	Long term
HeartMate II	TCI/Nimbus Inc./ Pittsburgh University, Pennsylvania USA	VAD/BTT	Implantable abdominal	Left/right ventricular	Long term
Impella	Impella, Cardiotechnik AG Aachen, Germany	Minimal invasive heart surgery	Fully implantable intraventricular	Left/right ventricular	Short term (< 6 h)
Valvo Pump	Keio University, Hokkaido University, Tokyo, Japan	VAD/similar to valve replacement	Implantable transvalvular	Left/right ventricular	Medium term
Streamliner	McGowan Center, Pittsburgh University, Pennsylvania USA	VAD/BTT	Implantable abdominal	Left/right ventricular	Long term

Table 1: Axial Blood Pumps [1]

VAD: Ventricular Assist Device; BTT: Bridge to transplant



Pump	Organization	Application	Position	Support	Duration
Bio-Pump	Medtronic Biomedicus Inc., Minneapolis,	Postcardiotomy/ CPB	Extracorporeal	Left/right ventricular	Short term
Capiox	Terumo Corporation Tokyo, Japan	CPB/postcardiotomy	Extracorporeal	Left/right ventricular	Short term
Sarns Delphin	Sarns/3M Health Care, Ann Arbor, MI, USA	Postcardiotomy	Extracorporeal	Left/right ventricular	Short term
Isoflow (Lifestream)	Bard Cardiopulmonar y Products/St Jude Medical Inc., Haverhill,	СРВ	Extracorporeal	Left/right ventricular	Short term
RotaFlow	JOSTRA Medizintechnik AG Hirrlingen, Germany	CPB/postcardiotomy	Extracorporeal	Left/right ventricular	Short term
Nikkiso	Nikkiso Co. Ltd Tokyo, Japan	СРВ	Paracorporeal	Left/right ventricular	Short term
HiFlow	HIA/Medos, GmbH Aachen, Germany	CPB/postcardiotomy	Extracorporeal	Left/right ventricular	Short term
Rotodynamic	Cleveland Clinic Foundation,	VAD	Implantable	Left/right ventricular	Long term
Gyro	Baylor College of Medicine, Houston, TX, USA	VAD /CPB	Implantable/ paracorporeal	Left/right ventricular	Long term to Medium term
AB-180	Cardiac Assist Technologies Inc. Pittsburgh, PA, USA	VAD postcardiotomy	Implantable/ Thoracic cavity	Left ventricular	Short term Medium term
Vienna	Vienna University Vienna, Austria	VAD	Implantable/ thoracic cavity	Left/right ventricular	Long term





Evaheart	Sun Medical Corp Pittsburgh University Japan/USA	VAD BTT	Implantable/ thoracic cavity	Left ventricular	Long term
Abiomed CF	Abiomed Inc., Danvers, MA, USA	VAD	Implantable	Left/right ventricular	Long term
Kriton	Kriton Medical Inc., Citrus Heights, CA, USA.	VAD	Implantable/ left ventricular apex	Left ventricular	Long term
MSCP	Terumo Corporation Setsunan University Japan	VAD	Implantable/ thoracic cavity	Left ventricular	Long term

# Table: 3 Diagonal pumps[1]

Pump	Organization	Application	Position	Support	Duration
VentrAssist	Micromedical Ltd, Sydney University, Australia	VAD/ BTT	Implantable/ abdominal	Left/right ventricular	Long term
HeartQuest	MedQuest Products Inc., Salt Lake City, UT, USA.	VAD/ TAH	Implantable/ Abdominal	Left/right ventricular	Long term (> 10 years)
DeltaStream	HIA/Medos, GmbH Aachen, Germany	CPB/VAD/ ECMO, etc.	Extracorporeal	Left/right ventricular	Short term



РИМР	WEIGHT/ SIZE	FLO W RAT E (L/M IN)	ROTATI ONAL SPEED (RPM)	POW ER REQ (WAT TS)	TYPES OF BEARI NGS	TYPE S OF SEALS	TYPES OF SENSOR S	ADDITIO NAL FEATUR ES	STAGE OF DEVELOP MENT
Hemopump	6g/5cc	4.5	25000	70	Purge fluid - lubricate d hydrostat ic journal bearings	Purged seal system Dextros e solutio n as purge fluid	External controller in console	Impeller (Archimed es screw) is driven by a flexible cable, which is rotated by a paracorpor eal motor Pump introduced through femoral artery Applicatio n in minimal invasive heart surgery Not produced anymore	Clinical use (since 1990)
Jarvik 2000	90g/25cc	6	10000- 160000	7-10	Blood- immerse d ceramic bearings	No seals	External microproc essor- based automatic motor controller regulating pump speed according to physical demands Control modes: Heart rate responsive mode or fixed rate mode possible	Rotor magnets inside impeller Electrical wires penetrate scalp Pediatric type available	Animal experiments
IVAP	170 g	5	9	8	Pressure- grooved ceramic journal bearings Bearings	First: purged - lip seal (silicon	External blood pump controller	Pump introduced through LV apex, outflow across	Animal expt

Table 4 : Detailed description of different types of axial pumps [1]



					cooled by purge fluid Bearings acting as a miniatur e viscous pump for the purge fluid (spiral/ helix grooves on bearings surface)	Later: Cool seal system		aortic valve	
DeBakye VAD	95g/ 15cc	5	7500- 120000	6	Ceramic bearings (blood lubricate d) located as the conjuncti on of the impeller with the flow straighte ner (front) and flow diffuser (rare)	No seals	Micro- controller coupled with internal battery powered by TETS	Rotor magnets are located (hermetica lly sealed) inside the impeller vanes CFD - based design Prices < USD 10000	Clinical trial
HeartMate II	160g/62cc	6	6000- 13000	10	Ceramic bearings, similar to ball cup jewel bearings, acting against radial and axial thrust Blood immerse d Ceramics and diamond coatings preferred bearing materials	No seals	Electronic ( external) controller modulates pump speed according to physiologi cal demands	Rotor magnets are located in the hub of the pumps rotor TETS will be used in the future	Ready for clinical trial
Impella	5g/2cc	4.5	30000	12	Ball bearings located inside motor chamber	Polyme ric lip seal	Internal pressure sensors for monitorin g, external controller integrade in console	Pump introduced through the femoral artery Integrated electric motor Long-term pump in developme	Clinical use



								nt	
								Price < US	
								\$1000	
Valvo Pump	138g/40cc	5	9000	26	Miniatur e ball bearings	Ferrofl uidic shaft seal Seal ring: Nd-Fe- B magnet Ferrofl uid: ferricol loid	Motor speed is determine d by counting pulses from the Hall sensors in the motor	\$1000Myocardiu m is used as pump housingPump may also be used in graftsMotor shaft is glued to the rotor	Laboratory
Streamliner					Magnetic ally levitated bearings Conical in shape Blood lubricate d and biocomp atible bearings	No seals	Internal and external controller coupled with TETS Hybrid controller architectur e	Computati onally optimized impeller geometry CFD- based design	Laboratory

Table 5: Detailed description of different types of centrifugal pumps [1]

PUMP	WEIGH T/SIZE	FLO W RAT E (L/M IN)	ROTATI ONAL SPEED (RPM)	POW ER REQ (WA TTS)	TYPES OF BEARINGS	TYPES OF SEALS	TYPES OF SENSORS	ADDITION AL FEATURE S	STAGE OF DEVELO PMENT
Bio- Pump	200g/87c c	6	5	8	Polycarbonate journal bearing	Flexible polymeric seal	Bio-console: electromagn etic flow measurement and pump speed controller	Rotating cone type pump Constraint force Vortex pump Bioactive surface available for improved biocompatibi lity BP- AT: Adult biopump BP50 pediatric biopump Frequently	Clinical use (greater than 20 years)

								used as reference pump for comparison studies	
Capiox	46cc	5	3000		Ball bearings	Polymeric lip seal	Auto flow cruise control system adjusts rotational speed to desired flow rate Ultrasonic Doppler flow meter.	Straight-path Rotor reduces pump speed without the decreasing hydraulic efficiency resulting in less hemolysis Rotor powered by magnetic coupling Automatic priming function allows pulsatile flow mode	Clinical use
Sarns Delphin	130g	9	3600		Ball bearings	Polymeric lip seal Problems with seal disruption encountered in clinical use	Microcompu ter-based control console Doppler flow sensor	Pulsatile flow mode option Open impeller with straight vanes Activated by magnetic coupling	Clinical use (greater than 10 years)
Isoflow	290g	9	3500		Sleeve bearings (sintered slide bearings) and ball bearings (axial thrust bearing)	Lip seal	Microproces sor-based system controller Reusable ultrasonic flow rate sensor	Open impeller with curved vanes Activated by magnetic coupling	Clinical use (> 10 years)
RotaFlow	35cc	10	4000		Magnetic stabilized rotor bearing (radial magnetic suspension) Low friction blood- immersed pivot bearing - sapphire ball (Al <sub>2</sub> O <sub>3</sub> ) and polyethylene calotte without shaft seals	No seals	Flow and bubble sensors in drive unit, pressure transducers Stand-alone console	Rotor powered by radial magnetic coupling Logarithmic spiral channels	Clinical use
Nikkiso	145g/25c c	10	36000	15	Ball bearings	V-shaped ring seal made of flurorubber	Ultrasonic flow meter External console	Activated by magnetic coupling Rotor driven	Clinical use



								by console through flexible shaft CFD studies on hemolysis Six straight vanes, six washout holes Two week with purging system washing the shaft-seal area Joint venture: Baylor College of Medicine has lead to Gyropump	
HiFlow	90g/30cc	6	3500	25	Spherical blood- immersed rotor thrust bearing . Ceramic- polymer bearing Minimal contact radius reduces heat generation within the bearing area	No seals	Pressure transducer and flow probe	Activated by magnetic coupling Pulsatile pumping option	Laboratory
Rotodynamic	207g/62c c	5	3000	6-7	Blood- lubricated hydrodynamic journal bearings Magnetic attraction between stator- rotor acts as thrust bearing	No seals	Flow rate proportional to heart rate determined by pacemaker	Grooved bearing surface provides a self- pumping action that generates wash flow Motor is surrounded by cooling blood flow TETS used for energy supply	Laboratory



Gyro	305g/145 cc	10	26000	7	Duoble pivot bearing system at top and bottom of impeller Blood- immersed bearings Alumina ceramic(Al <sub>2</sub> O <sub>3</sub> ) male pivot and polyethylene (UHMWPE) female pivot	No seals	Actuator controller	Eccentric inlet port eliminates obstacles in the blood path Activated by magnetic coupling GyroPI: Implantable- VAD GyroC1E3: Paracorporea I-CPB	Animal Expt
AB-180	284g/44c	6	4500	4	Bearings hydrodynamic journal bearing made of polycarbonate Lubricated and cooled by sterile water/ heparin infusion	Polyurethane - coated rubber seal	Microproces sor-based device regulates pump speed, infusion rate and occluder safety system	Balloon occluder system: Prevents back flow from aorta to let atrium if the pump fails Heparin infusion also used for anti- coagulation Rotor is powered by electromagn etic coupling	Clinical use
Vienna	240g/101 cc	6	2.5	15	Hybrid mechanical- magnetic bearing system (permanent magnets) Single mono- pivot mechanical support (ceramic/polye thylene)	No seal/shaft	Various controllers tested: Fuzzy non-linear and neuronal	Activated by magnetic coupling using double-disk motor Magnets used both for driving and bearing	Animal Expt
Evaheart	280g/150 cc	7	2500	9-10	Hydro dynamic journal bearing made of SiC Lubricated and cooled by purge fluid (sterile pure water) Viscous pumping effect by spiral grooves on bearing surface	Cool seal system: mechanical seal with circulating purge fluid	Ultrasonic flow measurement Thermocoup le meter for purge fluid temperature	Purge fluid continuously purified and sterilized by ultra filtration Diamond- like carbon coating	Animal Expt
Abiomed CF	190cc	10	3500	25 (15 for beari	Active magnetic suspension in combination	No seals/shafts	Analog electronic feedback control	Activated by magnetic coupling using an	Laboratory



Con the second				ngs)	with hydrostatic stabilization Electromagnet s as actuators Fluid between rotor and housing stabilize the magnetic suspension and contain axial motion		system for radial position Proximity sensors	internal motor More compact and efficient system in future design	
Kriton	195g/43c c	6	5000	6-10	Passive radial magnetic bearing acting in synergy with blood- lubricated hydrodynamic bearings eliminating the need for proximity sensors Blood- lubricated pivot bearing to constrain axial motion	No seals	Pressure meter and transonic flow probes	Activated by magnetic coupling Thick-bladed impeller due to imbedding of rotor magnets within the impeller blades	Laboratory
MSCP	400g/196 cc	5	2	15 (9 for magn etic suspe nsion )	Magnetic bearing Magnetic suspension of impeller providing contact free rotation Stainless steel motor bearings	No seals/shaft	Position sensors for magnetic suspension of bearings Sensor less system: No need for a flow pro, flow rate obtained through motor current	Activated by magnetic coupling Extracorpore al device available Future design: TETS, pulsatile mode, implantable controller	Animal Expt

PUMP	WEIGH T/SIZE	FL OW RA TE (L/ MI N)	ROTATI ONAL SPEED (RPM)	PO WE R REQ (WA TTS)	TYPES OF BEARINGS	TYPES OF SEALS	TYPES OF SENSORS	ADDITI ONAL FEATUR ES	STAGE OF DEVELO PMENT
VentrAssist					Magnetic suspension coupled with hydrodynamic bearing Fixed permanent magnets in upper and lower housing Passively suspended rotor	No seals	External controller worn on belt Sensor less motor control	Diagonal flow impeller activated by magnetic coupling CAD and CFD optimized system Vacuum- deposited coatings	Laboratory
HeartQuest	600g/275 cc	10	2500	6.5 for beari ngs	Hybrid magnetic bearing: actuators are a combination of permanent magnets and electromagnets (reduced power consumption) Full magnetic suspension	No seals/shaf t	Sensor less system, controller monitors motor current and determines pump speed Position sensors for bearings	Mixed flow impeller Motor integrated into the pump impeller and stator QuestCoat : flexible ceramic coating	Laboratory
DeltaStream	300g/150 cc	8	9000	40	Ball bearings located inside the motor chamber	Lip seal (polyuret hane)	Ultrasonic flow probe Hall sensor for motor speed Humidity sensor inside motor Temperature sensor on motor housing External console	Pulsatile flow option CFD studies Highly integrated design	Animal Expt

Table 6: Detailed description of different types of Diagonal pumps [1]

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Table 1 is the list of axial pumps available in the market where as table 3 describes three type of diagonal pumps that are available with their developers name. The axial blood pumps, centrifugal and diagonal pumps further charted into a table with more detailed format of their power requirements, type of sensors, rotational speed etc. This table of detailed data can be referred from tables 4, 5 and 6 [1] and can be used as literary reference for the study of different axial and centrifugal pumps.

#### **1.1. Need for improved design:**

With all the technological advance and availability of different tools for proper pump design, it is still important to build, test and then improve any design. Due to variable nature of the blood, it is very essential to build and test the pump design accurately. Despite of all these, rotary pumps have their own hazards such as shear rate compensation. Rotary pumps are best to obtain high flow rates, nearly 20L/min [1] but despite of all advantages, these pumps has limitations over the cavitations threshold and maximum allowable shear rates.

Hemolysis and platelet activation are affected by both shear stress and transition time in the pump [2]. In addition, blood trauma and blood cell destruction are most common. During the sealing, the heat generation also leads to local thrombus formation. These factors increase the risk of patient's life and also call for the need of technical solutions with improved quality of life. One of the major causes of death in USA is the Low output syndrome (LOS) after an open heart surgery. In addition to post- operational low output, cardiogenic shock or cardiac fibrillation also demands for more efficient means of cardiac assistive devices.



To avoid and reduce these causes due to traditional pumps, a pulsatilecontinuous flow pump design is considered [13]. The main aim of the pump is to provide a 20% cardiac assist to a person with congestive heart failures and other cardiac diseases. The pump under development is designed by utilizing a unique geometry and pumping actuation mechanism which helps to maintain low blood trauma, low anticoagulation levels preventing thrombosis and thus, less hemorrhage chances. This design also uses polyethylene oxide (PEO), a biocompatible material, which minimizes the protein interaction with the interior pumping surface thus reduces the coagulation of blood due to interaction.

The design utilizes biocompatible material, Polyethylene oxide (PEO), which minimized protein interaction with the interior pumping surface. Shape memory alloy actuators compress the pumping chamber. Shape memory alloy actuators also actuate compression of the ingoing sphincter valve and outgoing sphincter valves. Pumping motion can be analyzed by accelerometers to provide optimized feedback and pump motion control.



#### **CHAPTER 2**

#### **BLOOD RHEOLOGY**

The main concern of the project is to develop a design which can overcome the problems caused by the conventional pumps in the market. One of such problems is the hemolysis: the destruction of red blood cells causing the release of hemoglobin to the blood plasma. Hemolysis leads to platelet activation and thereby results in blood coagulation. Device induced platelet activation also leads to the consumption of anticoagulant drugs by the patient which over a period can cause internal bleeding. To help build an efficient design, one has to understand the fluid properties of blood.

When compared to water, blood is acts as a non-Newtonian fluid. The study of blood fluid dynamics has been carried out from a very long period to better understand the flow in arterial, venal and extracorporeal systems. Extensive study of the flow pattern and deformation of blood components is known as rheology. The deformation in case of blood refers to the viscoelastic behavior of blood.

As described earlier in chapter 1, most of the disadvantages of the current pumps lies in the vast abnormality of blood pattern. To get a pump to work without major drawbacks, one has to understand the components involved in the blood flow dynamics. The major factors affecting are blood plasma viscosity, RBCs (Red Blood Cells), WBCs (White Blood Cells), platelets, the hematocrit value of blood, fibrinogen and temperature.

#### 2.1. Blood behavoir:

Two study the fluid flow pattern of a blood we have to first understand the two main groups of liquid which are classified on the basis of viscosity and shear rate or



shear stress. First is Newtonian fluids in which viscosity is independent of the shear rate. Second is the non-Newtonian fluid in which viscosity may increase or decrease based on the shear rate. The magnitude of viscosity is calculated as the ratio of shear rate to shear stress. Shear stress is defined as the ratio of shear force to area.

Shear stress T = F/A (dyne/cm<sup>2</sup>)

In the study of fluid mechanics for a pipe with constant diameter and length, the resistance to flow depends on the flow conditions within the pipe. If the flow of fluid is slow then the pressure drop is proportional to the flow velocity. In this case the fluid particles move smoothly and parallel to the tube wall. Such a type of flow is called as laminar flow. On the contrary when the pressure drop in the tube is proportional to the square of the flow speed then the flow pattern is called turbulent which is a more chaotic form of flow. The resistance to flow is more in turbulent pattern when compared with the laminar flow.

#### 2.2. Newtonian and non- Newtonian Fluid:

As discussed earlier Newtonian and non-Newtonian fluids are the two classification of fluids which are based on the independency and dependency of viscosity on shear stress and shear rate respectively. In non-Newtonian fluids, the viscosity either increases or decreases with the increase in shear rate. As shown in figure 3 for Newtonian fluid, the slope of a shear stress versus shear rate graph gives a constant viscosity whereas for non-Newtonian fluid it varies along the graph. Non-Newtonian fluids have yield stress below which the shear stress is finite and the shear rate is zero giving an infinite viscosity condition. In case of blood if the yield stress is exceeded then the deformation of blood cells is irreversible leading to thrombosis.





Figure 3: Shear stress and shear rate relationship in Newtonian and non-Newtonian fluids

If the viscosity decreases with increase in shear rate, then the fluid is called shear-thinning fluid and if the viscosity increases with the increase in shear rate then it is called shear- thickening. Human blood behaves as a shear-thinning fluid with viscosity varying between 4 to 5 centipoise (cP) at 37°C when observed at high shear rate of 100 to 200 sec<sup>-1</sup>. With further increase in shear rate, viscosity becomes insensitive to shear rate. When the shear rate is reduced below 100 sec<sup>-1</sup>, viscosity increases exponentially with decrease in the shear rate.

The coefficient of viscosity,  $\eta$ , in fluid mechanics is given by the ratio of shear stress T to shear strain rate  $\gamma$  (also called velocity gradient):

 $\eta = T / \dot{\gamma} (dynes-sec) / cm^2 (poise)$ 



The steady state laminar flow can be given by Poiseuille's equation for a straight cylindrical tube:

 $Q = \pi * \Delta P * R^4 / L * 8\eta$  where Q is the flow rate,  $\Delta P$  is pressure difference, L is the length of the tube , R is the inner radius of the tube. This equation leads to the conclusion that for Newtonian fluids if the viscosity is doubled, the flow rate can be reduced to half and if the radius of the tube is doubled, it will lead to a 16 fold increase in the flow rate.

To experimentally measure the fluid viscosity of Newtonian fluids capillary viscometer is used, whereas to measure non-Newtonian fluid this instrument is not enough. Hence Couette viscometer, cone-in-cone viscometer or cone-on-plate viscometer is used. Despite of all these it is still difficult to study the rheology of human blood.

A small experiment where human blood was induced with ACD (anticoagulant citrate dextrose) solution a particular relationship between shear stress to shear strain rate was found which later developed as Casson's plot [11] as shown in figure 4 [8]. Casson's plot is also known as the double square root plot. It became apparent from these plots that blood behaves non-Newtonian near the origin implying that below 100 sec<sup>-1</sup> shear strain rate it obeys the non-Newtonian regime and after certain rate above that it obeys Newtonian regime. The Casson's plot curves derives the following relationship between shear stress (T) and yield stress (T<sub>y</sub>):

0-20 sec<sup>-1</sup>:  $T^{1/2} = T_y^{1/2} + \eta_N^{1/2} \dot{\gamma}^{1/2}$ 

above 100sec<sup>-1</sup>:  $T^{1/2} = \eta_N^{1/2} \dot{\gamma}^{1/2}$  or  $T = \eta_N \dot{\gamma}$  where  $\eta_N$  is the ultimate Newtonian viscosity and  $\dot{\gamma}$  is the shear strain rate. Hence blood exhibits a viscoelastic behavior with the non-Newtonian property more dominating.





Figure 4: Non- Newtonian shear stress and shear strain rate along with Casson's Plot [8]

#### 2.3. Blood components:

#### 2.3.1. Blood plasma:

Plasma is the suspension portion of the blood which contains the RBCs, WBCs and platelets along with other proteins and salts. The normal range of blood plasma viscosity varies between 1.10 and 1.35 centipoise(cP) [6], [7]. The change in plasma viscosity directly affects the blood viscosity value. This change is irrelevant to the hematocrit value and the other cellular elements. Studies have shown that plasma acts as a Newtonian fluid but the presence of elements in it makes it to behave as non- Newtonian.

# 2.3.2. RBC aggregation and deformation:

The pattern of flow streamlines depend on the concentration of RBCs and the deformation of these cells under pressure, specifically shear forces. RBCs affects the flow of



blood in a vessel by either subjecting itself to sedimentation against gravity or the densification process thereby increasing the hematocrit value[9].

Healthy RBCs easily responds to applied forces and gets deformed with changes in their shape. RBCs have biconcave disk shape which also behave as elastic bodies. Generally the deformation is reversible but in cases of increased shear rate, the change happens for permanently. Due to the shape change and applied pressure, the RBCs aggregate to form linear arrays in the form of stack of coins, termed as rouleaux. These further aggregate to form 3D structures. The aggregate formation increases the blood viscosity to a great extent.



Figure 5: Relationship between the viscosity of blood and the shear rate [6]



Within normal blood parameters, the aggregation process is in balance with disaggregating forces. An increase in the shear rate disintegrate the aggregates and a reduction the shear rate would increase the aggregate formation(9). Figure 5[6] gives an overview of the aggregation and deformation curve with applied shear rate.

#### 2.3.3. Hematocrit:

Hematocrit is the value which gives the measure of red blood cells in the blood by percentage volume. It defines the packed RBC cell volume. This value varies differently for men and women from a range of 40.7 -50.3 %, 36.1-44.3%, respectively. Figure 6 [1] [6] shows the correlation between the viscosity and the hematocrit value of blood.



Figure 6: Graph showing relationship between blood viscosity and hematocrit value. [1] [6]
It can be observed from figure 6 [1] [6] that there is an exponential increase in the value of viscosity with an increase in the hematocrit value. There is an increase of 4% in blood viscosity for a unit increase of hematocrit at medium to high shear rates. The relation between hematocrit H and plasma viscosity n<sub>p</sub> can be given as



 $\eta_N = \eta_P \ \{ \ 1+ \ 0.025 H + \ 7.35 \ * \ 10^{-4} \ H^2 \} \text{ where } \eta_N \text{ is the ultimate Newtonian}$  viscosity over a range of  $\eta_N$  ranging from 0.03 P at hematocrit of 40 to 0.10 at hematocrit 65 [8].

For non- Newtonian regime, the yield stress  $(T_y)$  is best correlated with hematocrit over a range to 30-50 with the following equation:

 $T_y = A (H-H_c)^3$  where A is constant ranging between 0.6-1.2 \* 10<sup>-6</sup> and H<sub>c</sub> is the limiting hematocrit between 4 and 8. The value of A is highly dependent on the fibrinogen concentration. At a hematocrit of 40 the yield stress value is typically 0.04 dyne/cm<sup>2</sup>. With an increase in the hematocrit value above 50, the blood displays various rheological abnormalities.

## 2.3.4. Fibrinogen:

As stated above the fibrinogen concentration plays a major role in the blood viscosity determination. The fluid pattern of blood heavily depends on the red blood cell and fibrinogen interaction. The variation of yield stress  $T_y$  and fibrinogen concentration  $C_f$  can be given by the equation

$$T_y = B C_f^2$$

where B is a constant varying between  $1 * 10^{-11}$  to  $2 * 10^{-11}$  and weakly depends on the concentration of other proteins in the blood plasma. This equation is valid over a range of 100-400 mg% concentration of fibrinogen [8].

# 2.3.5. Temperature:

When blood follows the range of Newtonian fluid, it is observed that the temperature coefficient of viscosity is same as that of water over a range of 10-37 C [10]. In the non-Newtonian range , the viscosity and fluid flow are less affected by the temperature.



For 90% of human subjects the yield stress was independent of temperature but for the rest of 1% there was a small increase in the yield stress with a decrease in the temperature.

#### 2.3.6. WBCs and Platelets:

Generally WBCs and platelets does not contribute to the macroscopic fluid properties of blood due to the less concentration of these components as compared to the RBCs present. These although influence the blood flow resistance in microcirculation.

## 2.3.7. Thrombosis:

Thrombosis in general terms is the clotting of blood. Blood clotting in the pumps is a major factor of pump failure. Thrombosis happens as a result of red blood cell aggregation at high shear rates which induces the activation of platelets and fibrin forming first a mesh like structure leading to the clot formation. Thrombosis results in the increase in the blood viscosity which in some cases leads to clotting of remaining blood in contact.

# 2.4. Effect of fluid mechanics on pump development:

While design the pump we have to keep in consideration the semi Newtonian and non-Newtonian fluid pattern of the blood along with all the above mentioned factors affecting the viscosity of blood. Since the pump acts on the arterial blood pressure, the flow velocity becomes sufficiently high indicating that the shear stress corresponds to the Newtonian part of the blood fluid dynamics. The viscosity of blood flowing through tubes having smaller diameter reduces and as the diameter decreases further, the viscosity value increases sharply.

Also the hematocrit value of blood inside the tube is less and the hematocrit value at the discharge outlet i.e., at outflow is more. During the flow of blood through a vessel two major factors affect the blood viscosity thereby leading to clot formation: a) the


sedimentation of red blood cells due to effect of gravity to the vessel lining, b) when in vertical position due to axial movement of red blood cells in the vessel, flow resistance is reduced leading to low viscous regions near the tubes of the vessel wall. Hence blood flow velocity and pumping efficiency depends on the aggregation and deformability capacity of red blood cells, sedimentation property due to orientation of pump and gravity, tube diameter, fibrinogen to fibrin formation.

Also lysed red blood cells, free hemoglobin in plasma and presence of air bubbles affects the pump function. Lysed red blood cells comes in contact with healthy cells and thereby activates fibrinogen forming aggregates of these lysed (ghost) cells. If the free hemoglobin concentration in the plasma increases then it results in the increase of yield stress. The chance of developing air bubbles in the pump can have a lethal impact on the person as it leads to hemolysis: the breaking of red blood cells releasing the hemoglobin into blood plasma which induces a reaction chain of thrombosis and embolization (formation and circulation of embolus, an intravascular mass) . Understanding these factors help in the development of a better pulsatile pump although in-depth apprehension of blood rheology still needs to be carried out.



#### **CHAPTER 3**

#### **DESIGN PRINCIPLE AND WORKING**

#### 3.1. Design:

As discussed in the previous chapters the major hurdle in the development of the pump is to design a model which can minimize the shear stress and therby can reduce the blood cell damage it causes. To achieve such a design different design prototypes were considered with extensive research and one working design is proposed which considers the principle of a low shear pump and utilizes a unique geometry and pumping actuation mechanism.

The proposed working prototype of the pump was created using AutoCAD. The following figures shows the front view and side views of the pump.



Figure 7: Front view of the proposed pump





Figure 8: Side views of the pump design.

To validate the two dimensional design, we needed to study the volume covered inside the tube, flow obtained and which pattern of flow is observed. To understand the volume contained by our design mathematical calculations can be used. The pump design can be approximated to the combination of two cylinders with an ellipsoid. Now the



total volume contained inside the pump will be the addition of volume of two cylinders and the volume of ellipsoid.

Volume of pump= 2\* volume of cylinder + volume of ellipsoid

$$= 2 * \pi^{*}(4.5)^{2}(25) + 4/3 * \pi^{*} 50/2 * 30.2/2 * 30.2/2$$
$$= 2 * 1590.43 + 23865.0467 \text{ mm}^{3}$$
$$= 2 * 1.59 + 23.86 \text{ cm}^{3} \text{ (approx)}$$
$$= 27.04 \text{ cm}^{3} \text{ (approx)}$$

Now this implies 0.027 liters per sec . So the per minute output will be (1.59+23.86)cm<sup>3</sup> \* 60 minute. this can be equated to :

Volume flow out = 25.45 cm<sup>3</sup> \*60/ minute

So this falls under the proposed domain of the output that the design produces. Also to validate the design technical aspects and to check whether the design produces a flow patter in the laminar flow range we calculated the Reynolds number at the output of the pump. In general, Reynolds number =  $\rho QD/\mu A$  where  $\rho$  is the density of blood (1060 kg/m<sup>3</sup>), Q is the flow rate, D is the diameter of the tube,  $\mu$  is the dynamic viscosity of blood (3.5\*10<sup>-3</sup> Pa.s) and A is the cross sectional area of the tube.

Reynolds number=  $(1060 \times 25.45 \times 10^{-6} \times 0.009)/3.5 \times 10^{-3} \times \pi \times 0.009(4.5 \times 25) \times 10^{-3}$ 

= 83.2 (approx), showing that the flow obtained at the end is a laminar

flow.

A three dimensional figure of the model was created which shows the pump as a whole with its input and output outlets. Figure 9 shows the 3D picture depicting the



sphincters and valves of the pump. Figure 10 and figure 11 shows the two dimensional cut section and the layer section of the pump.



Figure 9 : Three dimensional model of the proposed pump



Figure 10: The two dimensional cut section





#### Figure 11: Layer section of the pump

After the two dimensional and three dimensional design manifestation, to aid this design the flow dynamics of the model is studied using COMSOL simulation.

#### 3.2. Principle:

The design and working principle of the pump are developed by considering all the major factors affecting the current pumping and assistive systems. The main principle involved in the design of the pump is the implementation of the pulsatile motion into the pump which biomimics the actual heart compression and pulsation. The duty of the pump is to provide assistance to a weak pumping heart. After studying the arterial pressure and cardiac output of the heart, the blood flow was stated according to the Darcy's Law of calculating Mean Arterial Pressure (MAP). According to this law :

#### MAP = CO\*SVR + CVP

where CO is cardiac output, SVR is systemic vascular resistance, CVP is central venous pressure. This equation can be simplified as MAP ~  $P_{dias} + 1/3 * (P_{sys} - P_{dias})$ , where  $P_{dias}$  is diastolic pressure and  $P_{sys}$  is the systolic pressure. For patients having low



pumping pressure and to increase the blood pressure, the pump would provide an increase of 20% to blood pressure by pumping the blood from the venous supply to the arterial supply as seen from figure 12. For this purpose the blood pumping flow rate should reach the 20% of the normal rate, which make the proposed pump to produce a flow rate in between 1L/min to 2L/min.

As discussed in the earlier chapter the high speed rotation pumps and displacement pumps produces high shear stress which cause blood thrombosis and embolization. So the pump design has to be a prototype which causes low blood damage and to achieve this, pulsatile pumping motion mimicking the actual heart compression and decompression process is used.



Figure 12: Proposed positioning of the pump in development.

The pump has a minimum pressure capacity of 120 mmHg at 50 to 150 heart beats per minute. Since the pump design provides 50 to 120 beats/minute, the average number of times it beats per minute can be calculated as: 50+120/2=85 beats (average)/min.



Therefore, time taken for one beat will be: 60/85= 0.7058 sec approximately. Process of compression and decompression relates to one complete cycle of pump. So compression and decompression takes half of the pump cycle respectively. Therefore time taken to compress could be approximated as 0.7058/2= 0.3529 sec. Similarly the time taken to decompress also approximates to 0.3529 sec. This pressure can be measured using blood pressure sensors or direct electro cardiac sensing. This pumping principle provides a wide variety of applications not just limited to the arterial pumping.

#### **3.3 Working Mechanism:**

As described in the principle, the proposed pump works on the pulsatile compression an d decompression mechanism of the heart. The design follows unique geometry where we first study the flow and fluid dynamics using simulation techniques. The proposed theory of pump can use shape memory alloy actuators which helps in the compression of the pumping chamber. Also pneumatic cuffs can be used to inflate and deflate the pump body. These cuffs also control the compression of the sphincters attached at the input and the output which are used to minimize the thrombosis caused by turbulence. Although shape memory actuators can also be used, the design with pneumatic cuffs has been studied as it helps simple sequencing of the two-way valve.

Figure 13 shows the prototype model using the pneumatic cuffs for the compression and decompression of the pump. The pump follows a basic mechanism: as the blood flows in through the input, the input valve opens creating the pump chamber to inflate and then as soon the chamber fills in, pressure builds up causing the input valve to close and the output valve opens which thereby results in the compression of the pump and output flow of blood. To achieve sequential actuation of complex and continuous flow pattern in the



pump, a cluster of pumps (each independently controlled) can be packaged together with low turbulence flow. This type of zonal compression allows optimal compression for blood flow.



Figure 13 : A pneumatic version of the pumping apprentice. (1) outgoing sphincter valve controlled by pneumatic cuff, outer titanium case, (3) main pump pneumatic cuff actuator, (4) polymer pump body with PEO lining, (5) inlet sphincter valve cuff, (6) 6-axis accelerometer chips for actuation analysis, (7) pneumatic control lines, (8) valve to control actuation, (9) pneumatic pump (saline or gas).

### 3.4. Simulation:

As described earlier, to fully understand the mechanism of fluid flow of the proposed pump design and to aid the design development, the simulation study of the pump is conducted through COMSOL multiphysics software. To better understand the fluid flow properties a peristaltic model is stimulated which can help understand the stress applied on the fluid and to observe the velocity field of the flow in the pump.



In the developed model, the flow of fluid is through a cylindrical pipe and external pressure is applied which leads to the deformation of the tube thereby creating stress in the fluid. The simulation consist of transient analysis based on incompressible Navier-Stokes equation which is given by

$$\rho \frac{\partial \mathbf{u}}{\partial t} - \nabla \cdot \eta (\nabla \mathbf{u} + (\nabla \mathbf{u})^{T}) + \rho \mathbf{u} \cdot \nabla \mathbf{u} + \nabla p = 0$$
$$\nabla \cdot \mathbf{u} = 0$$

where P is density (kg/m<sup>3</sup>), **u** is flow velocity (m/s),  $\eta$  is viscosity (Pa.s) and p is pressure. The model uses simple geometric construction of a rectangle to model a cylinder as seen from figure 14 and has a set of constants tabulated in table 2.



Figure 14: Geometric model construction

The model use three application modes: axial symmetry, stress-strain ; moving mesh and incompressible Navier- Stokes system. Hence this model becomes a combination of structural mechanics and fluid dynamics. The moving mesh application is used to study the deforming geometry of the model.



Name	Expression	Value	Description
t_on	0.3[s]		Time when roll is engaged
t_off	1.2[s]		Time when roll is disengaged
dt	0.2[s]		Time to reach full force
z0	0.03[m]		z coordinate where roll starts
v0	0.03[m/s]		Vertical velocity of roll
width	0.01[m]		Width of Gaussian force distribution
Ttot	1.5[s]		Total time for a pump cycle
Lmax	4e6[N/m^2]		Max load

 Table 7: Set of Constants used for modeling

For developing the fluid simulation, the boundary conditions at the inlet and outlet of the pump assumes that :

$$\mathbf{n} \cdot [-pI + \eta (\nabla \mathbf{u} + (\nabla \mathbf{u})^T)] = \mathbf{0}$$

This implies that the total stress at the inlet and the outlet of the pump is zero. While configuring the moving mesh, it is fixed to a zero *r* displacement at the symmetry axis and at the top and bottom of the tube it is at a zero *z* displacement. To obtain the volumetric flow rate ( $\dot{V}$ ) in m<sup>3</sup>/s at the input and output is given by

$$\dot{V}_{\text{in}} = -\int_{s_{\text{in}}} 2\pi r(\mathbf{n} \cdot \mathbf{u}) ds$$
$$\dot{V}_{\text{out}} = \int_{s_{\text{out}}} 2\pi r(\mathbf{n} \cdot \mathbf{u}) ds$$

where **n** is the outward-pointing unit normal and s is the boundary length parameter. Similarly the total volume of the fluid in  $m^3$  can be calculated using



$$V = \int_{A} 2\pi r dA \qquad V_{\text{pump}}(t) = \int_{0}^{t} \dot{V}_{\text{out}} dt$$
$$\frac{dV_{\text{pump}}}{dt} = \dot{V}_{\text{out}}$$

where A is the deformed domain.  $V_{pump}$  is the volume of fluid that comes out through the outlet. The derivative equation is then used to derive the above stated integral. The boundary conditions for the model are set accordingly and a major equation is used to set the edge load i.e. the load or the decompression on the pump. The load acting is force per unit area with a boundary setting of  $\{-Lmax*flc2hs((t-t_on)[1/s], dt[1/s])*gauss((z 0.05)[1/m],width[1/m])*flc2hs((t_off-t)[1/s],dt[1/s])\} where the middle factor plays a major$ role in the positioning of the pressure. In the simulation we apply the load at the midpoint ofthe tube.



Figure 15: End result of simulation depicting the load applied



Figure 15 shows the end result of the simulation with the velocity - deformation profile. A full detailed report of the simulation with all the tables and boundary conditions are provided in Appendix 2.



#### **CHAPTER 4**

#### MATERIAL USED

The material used to develop the inner sheathing of the pump is implant grade liquid silicone rubber (LSR). Liquid silicone rubber is a curated silicone with high purity platinum at low compression set properties which has more stability towards extreme temperature variation from hot to cold and can also be molded into various wall thickness within a same part - a requirement for the production of high quality parts.

#### 4.1. Chemical background and uses:

Liquid silicone rubber belongs to a family of thermoset elastomers with a chemical backbone of alternating silicon and oxygen atoms with methyl or vinyl side groups. The methyl group in the side chains contribute to the hydrophobicity of the material. The LSR used in the project has dimethyl chains. LSR has been specially used by the medical device manufacturers to produce more stable, flexible and physically implantable quality products. Some of the application of silicone rubber is in the manufacturing of precision molded parts, diaphragms, septa, valves, plungers etc. Since platinum cured, the rubber has long shelf life with excellent chemical resistance.

#### 4.2. Basic properties:

LSR used in the molding procedure was manufactured by Applied Silicone Corporation. The LSR came in two parts A and B, both being colorless, translucent and ultraviolet- and strain resistant. The material has the property to withstand high strength which is basic requirement for the pump development. To obtain the elastomer of desired toughness and rubbery texture both the parts A and B (figure 16) are to mixed in equal



proportion [12]. Despite of its virtual unlimited shelf life, the manufacturer suggest a shelf life upto 3 years for molded parts. The specific material used for the project from Applied Silicone Corporation has long term implantation capacity with high durability.





One of the eye catching property of LSR is its biocompatibility. It is also hypoallergenic which implies that the implanted device or part will have minimum risk of developing an allergic reaction in the host body. It also has anti-bacterial and fungal properties resulting in minimal chances of developing any bacterial or fungal infections in the body. LSR belongs to a family of thermosets resulting in its property of withstanding wide range of temperature change ( -55°C to 200°C) allowing it to go through sterilization processes like autoclaving without changing its properties.

### 4.3. LSR usage in laboratory:

When mixed part A and part B in a 1:1 ratio under proper conditions and with required specific inner dimensions of the pump, two molds were made.



Figure 17 shows the molds made in the laboratory to study the device inner dynamics.

Figure 17: The two inner surface moulds made out of LSR

Further specific details of the properties of LSR from applied silicone corporation can be referred by the material safety data sheet (MSDS) of LSR systems from Appendix 1.



#### **CHAPTER 5**

#### **DISCUSSION AND CONCLUSION**

A potential working prototype of a heart mimicking pump have been proposed. To overcome the disadvantages of the current pumps available in the market, different actuation methods and blood fluid dynamics have been studied. A vast majority of heart assist devices are complete bypass or large volume pumps that can cause significant blood cell damage which results in the thrombosis and thereby causes blood clotting and increases stroke/ heart failure chances.

The proposed design of the pump works on the basis of mimicking the actual heart pumping mechanism: the pulsatile compression and decompression. This mechanism helps in achieving the required flow rate with a less turbulent blood flow resulting in minimal blood cell damage. The pump under development focuses a lot on the prevention of damage to the blood cells due to the turbulent flow of blood in other rotary and displacement pumps. The pumping action of the device is created by the pressure gradient against the continuous flow. In general, continuous flow pumps produces non-pulsatile flow using a rotor which generally contains magnets that leads to a turbulence in the blood.

The use of COMSOL simulation has aided to the better understanding of the design and the blood flow dynamics. The studies through COMSOL simulation has suggested that the proposed design provides a lesser shear rate as compared to other heart assist devices which added as an advantage. The design also includes sphincter-like valves that also helps minimize the thrombosis which in other pumps is a result of turbulence. The design takes special care into the biocompatibility of the material used and in order to



achieve this, it is can be coated with a layer of polyethylene oxide (PEO) which reduces the protein interaction on the pump interior surfaces.

The actual compression and decompression of the pump caused by the sphincter valves are controlled by pneumatic cuffs. To improve the design capacities both shape memory alloys and pneumatic cuffs implementation has been studied. The pneumatic cuffs around the pump can help in the inflation and the deflation of the sphincter valves. This results in a zonal compression of the pump which give an optimized blood flow rate. Further research has been carried out with the prototype having pneumatic cuffs rather than shape memory alloys as it provides simple sequencing on the two way valves. Accelerometers are incorporated to the design that analyses the pump body motion and can provide a feedback of the pumping action. Further a cluster of pumps can be packed together to obtain complex flow patterns.

This blood pump design can provide upto 20% of cardiac assist to persons suffering from congestive heart failure and other heart abnormalities where extra blood pumping assistance is required. The pump also has minimum pressure capacity of 120mmHg at 50-150 heart beats per minute. Also the design suggested and in development have a broad spectrum of uses. This design is not just limited to the arterial to arterial pumping but can be used for physiological fluidic maintenance, intravenous drug delivery and pressure maintenance and to other applications where a low turbulence and shear stress is required.



#### **APPENDIX 1**

#### MATERIAL SAFETY DATA SHEET

#### LIQUID SILICONE RUBBER (LSR) SYSTEMS

### I. PRODUCT IDENTIFICATION

A. Manufactured by:

APPLIED SILICONE CORPORATION

270 QUAIL COURT

SANTA PAULA, CA 93060

Telephone: (805) 525-5657

Fax: (805) 933-1675

For Chemical Emergency Please call CHEMTREC (800) 424-9300

- B. Trade Name: Liquid Silicone Rubber (LSR), Part A and Part B
- C. Chemical Name and Synonyms: Part A: reinforced dimethyl methylvinyl siloxanes. Part B: reinforced dimethyl methylhydrogen siloxanes.
- D. Chemical Formula: N/A (polymeric), both Part A and Part B.
- E. Chemical Family: Part A: reinforced organopolysiloxane, Part B: organopolysiloxane
- F. DOT (CFR 49) Hazard Classification: Not hazardous per CFR 49

### II. PRODUCT COMPOSITION

Dimethyl Silicone Elastomer Base, 100%

### III. PHYSICAL PROPERTIES – PART A

- A. Boiling Point: >260 °C
- B. Specific Gravity (water = 1): 1.1
- C. Vapor Pressure at 25 °C: >1 mm Hg essentially non-volatile
- D. Vapor Density (Air = 1): N/A essentially non-volatile
- E. Water Solubility: nil
- F. Evaporation Rate (Ethyl Ether = 1): nil
- G. Appearance and Odor: Colorless, translucent, viscous, paste



### **III. PHYSICAL PROPERTIES - PART B**

- A. Boiling Point: >260°C
- B. Specific Gravity (water = 1): 1.1
- C. Vapor Pressure at 25°C: negligible essentially non-volatile
- D. Vapor Density (Air = 1): N/A essentially non-volatile
- E. Water Solubility: nil
- F. Evaporation Rate (Ethyl Ether = 1): N/A
- G. Appearance and Odor: Colorless, translucent, viscous, paste.

#### IV. FIRE AND EXPLOSION INFORMATION – PART A AND PART B A. Flash Point (Open Cup): Part A: 190°C; Part B: 95°C

- B. Flammable Limits in Air, % Volume: Not measured
- C. Extinguishing Media: Use water fog, dry chemical, foam, or CO<sub>2</sub>
- D. Special Fire Fighting Procedures: Fire fighters should wear self-contained breathing apparatus and full protective clothing. Use water spray to cool nearby containers.
- E. Unusual Fire and Explosion Hazards: Part B may generate Hydrogen gas to create an explosion hazard.

### V. HEALTH HAZARD AND PROTECTION DATA - PART A AND PART B

- A. Personal Protection Recommended: Wear protective goggles to prevent eye contact. Under recommended conditions of use, no other protection should be required.
- B. Signs and Symptoms of Exposure: The primary route of exposure is eye contact. Direct eye contact can cause a transitory irritation, but it is not injurious. This irritation may persist for up to 24 hours.

Experience with this material has not indicated any serious effects related to exposure by any route.

- C. First Aid for Exposure:
  - 1. Eye contact: Flush with water. Get medical attention if irritation persists.
  - 2. Skin contact: Not considered a potential hazard. If irritation occurs, wash thoroughly with soap and water.
  - 3. Ingestion: Get medical attention
  - 4. Inhalation: Not considered a potential hazard.



- D. Occupational Exposure Limits: Because of the low health hazard, no exposure limits have been established.
- E. Eye irritant in raw state.
- F. Medical Conditions Generally Aggravated by Exposure: Pre-existing eye disorders.
- G. Toxicity: Because of the low toxicity, specific toxicity data is unavailable.

#### VI. SPILL AND LEAK PROCEDURES - PART A AND PART B

Use personal protection recommended in section V to prevent personnel exposure.

Even small amounts of spilled material may present a slip hazard.

As required, dike with soil or other absorbent materials to prevent spread of spill. Mop or wipe up and place in appropriate containers and/or place absorbent material on spill and transfer absorbed solvent to appropriate containers. Clean any remaining slippery surfaces. Mop or swab with appropriate solvent or wash with mild caustic detergents.

#### VII. REACTIVITY DATA - PART A AND PART B

- A. Stability: This material is chemically stable. Hazardous polymerization will not occur.
- B. Materials to Avoid: Strong alkali contact with Part B may generate flammable hydrogen gas.
- C. Hazardous Decomposition Products: Burning may liberate carbon monoxide, carbon dioxide and silicone dioxide.

### VIII. OTHER INFORMATION AND PRECAUTIONS - PART A AND PART B

Store in a cool, dry place. Keep container closed and keep away from heat and flame. Do not lay container on its side.

To the best of our knowledge this material does not contain any substances listed by the state of California to cause cancer, birth defects, or other reproductive effects.

When this material is discarded, as received, it is not classified as a RCRA hazardous waste. state and local laws may impose additional regulatory requirements regarding disposal.

Consult and comply with federal, state, and local regulations concerning any release of hazardous materials into the water, water piping systems, ground, or air. Consult and comply with federal, state, and local regulations concerning removal of waste.

All information appearing herein is based upon data considered to be accurate. However, no warranty is expressed or implied regarding the accuracy of these data or the results to be obtained from the use thereof.



### **APPENDIX 2** COMSOL SIMULATION RESULT

**1. Model Properties** 

Property	Value
Model name	Peristaltic Pump
Author	COMSOL
Company	COMSOL
Department	
Reference	Copyright (c) 1998-2008 by COMSOL AB
URL	www.comsol.com
Saved date	Apr 10, 2015 2:16:34 PM
Creation date	Nov 17, 2008 7:12:05 PM
COMSOL version	COMSOL 3.5.0.603

Application modes and modules used in this model:

- Geom1 (Axial symmetry (2D))
  - Axial Symmetry, Stress-Strain
  - Moving Mesh (ALE)
  - Non-Newtonian Flow (Chemical Engineering Module)

## 1.1. Model description

#### Peristaltic Pump

Rollers are squeezing a flexible tube in this model of a peristaltic pump. The compression drives a fluid through the tube. The motion of the fluid is computed with the help of a Moving Mesh application mode.

### 2. Constants

Name	Expression	Value	Description
t_on	0.3[s]		Time when roll is engaged
t_off	1.2[s]		Time when roll is disengaged
dt	0.2[s]		Time to reach full force
z0	0.03[m]		z coordinate where roll starts
v0	0.03[m/s]		Vertical velocity of roll
width	0.01[m]		Width of Gaussian force distribution
Ttot	1.5[s]		Total time for a pump cycle
Lmax	4e6[N/m^2]		Max load



# 3. Geometry

Number of geometries: 1

## 3.1. Geom1









## 3.1.2. Boundary mode



## 3.1.3. Subdomain mode





### 4. Geom1

Space dimensions: Axial symmetry (2D) Independent variables: R, PHI, Z

#### 4.1. Mesh

### 4.1.1. Mesh Statistics

Number of degrees of freedom	7741
Number of mesh points	517
Number of elements	916
Triangular	916
Quadrilateral	0
Number of boundary elements	166
Number of vertex elements	6
Minimum element quality	0.924
Element area ratio	0.398







### 4.2.1. Application Mode Properties

Property	Value
Default element type	Lagrange - Quadratic
Analysis type	Transient
Specify eigenvalues using	Eigenfrequency
Frame	Frame (ref)
Weak constraints	Off
Constraint type	Ideal

## 4.2.2. Variables

Dependent variables: uor, w Shape functions: shlag(2,'uor'), shlag(2,'w') Interior boundaries not active

### 4.2.3. Boundary Settings

Boundary		4	5- 6	7
Edge load (force/area) R- dir. (Fr)	N/m <sup>2</sup>	0	0	-0.5*Lmax*flc2hs((t-t_on)[1/s],dt[1/s])*gauss((z- 0.05)[1/m],width[1/m])*flc2hs((t_off-t)[1/s],dt[1/s])
Hr	1	0	1	0
Hz	1	0	1	0

### 4.2.4. Subdomain Settings

Subdomain		2
Young's modulus (E)	Pa	2e9[Pa] (Nylon)
Density (rho)	kg/m <sup>3</sup>	1150[kg/m^3] (Nylon)

### 4.3. Application Mode: Moving Mesh (ALE) (ale)

Application mode type: Moving Mesh (ALE) Application mode name: ale

### 4.3.1. Application Mode Properties

Property	Value
Default element type	Lagrange - Quadratic
Smoothing method	Winslow



Analysis type	Transient
Allow remeshing	Off
Defines frame	Frame (ale)
Original reference frame	Frame (ale)
Motion relative to	Frame (ref)
Weak constraints	On
Constraint type	Non-ideal

### 4.3.2. Variables

Dependent variables: Shape functions: shlag(2,'lm3'), shlag(2,'lm4'), shlag(2,'r'), shlag(2,'z') Interior boundaries not active

### 4.3.3. Boundary Settings

Boundary			1	2-3	4
Туре			Mesh displacement	Mesh displacement	Mesh displacement
Mesh (deform)	displacement	m	{0;0}	{0;0}	{uaxi_axi;w}
defflag			<b>{1;0}</b>	<b>{0;1}</b>	{1;1}

## 4.3.4. Subdomain Settings

Subdomain		1				2
Shape functions (shape)		shlag(2,'lm3') shlag(2,'lm4') shlag(2,'r') shlag(2,'z')			'lm4')	shlag(2,'lm3') shlag(2,'lm4') shlag(2,'r') shlag(2,'z')
Integration order (gporder)		4 4				4 4
type		Free displacement			Prescribed displacement	
Displacement expressions (presexpr)		{0;0}			{uaxi_axi;w}	
Subdomain initial value			1	2		
Spatial coordinate (r)		m	rinit_ale	rinit_ale		
Spatial coordinate (z)		m	zinit_ale	zinit_ale		



### 4.4. Application Mode: Non-Newtonian Flow (chns)

Application mode type: Non-Newtonian Flow (Chemical Engineering Module) Application mode name: chns

#### 4.4.1. Scalar Variables

Name	Variable	Value	Unit	Description
visc_vel_fact	visc_vel_fact_chns	10	1	Viscous velocity factor

### 4.4.2. Application Mode Properties

Property	Value
Default element type	Lagrange - P <sub>2</sub> P <sub>1</sub>
Analysis type	Transient
Corner smoothing	Off
Weakly compressible flow	Off
Turbulence model	None
Realizability	Off
Non-Newtonian flow	On
Brinkman on by default	Off
Two-phase flow	Single-phase flow
Swirl velocity	Off
Frame	Frame (ale)
Weak constraints	On
Constraint type	Ideal

### 4.4.3. Variables

Dependent variables: u, v, w2, p, logk2, logd2, logw2, phi2, psi2, nrw2, nzw2 Shape functions: shlag(2,'lm5'), shlag(2,'lm6'), shlag(1,'lm8'), shlag(2,'u'), shlag(2,'v'), shlag(1,'p') Interior boundaries not active

### 4.4.4. Boundary Settings

Boundary	1	2-3	4
Туре	Symmetry boundary	Open boundary	Inlet
velType	U0in	U0in	u0



r-velocity (u0)	m/s	0	0	uaxi_t_axi
z-velocity (v0)	m/s	0	0	wt

## 4.4.5. Subdomain Settings

Subdomain		1
Shape functions (shape)		shlag(2,'lm5') shlag(2,'lm6') shlag(1,'lm8') shlag(2,'u') shlag(2,'v') shlag(1,'p')
Integration order (gporder)		4 4 2
Constraint order (cporder)		221
Model parameter (m)		0.0161
Model parameter (n)	1	.63
idon		1
cdon		0

# 5. Materials/Coefficients Library

## 5.1. Nylon

Parameter	Value
Heat capacity at constant pressure (C)	1700[J/(kg*K)]
Young's modulus (E)	2e9[Pa]
Thermal expansion coeff. (alpha)	280e-6[1/K]
Relative permittivity (epsilonr)	4
Thermal conductivity (k)	0.26[W/(m*K)]
Density (rho)	1150[kg/m^3]

## 6. Global Equations

Name (u)	Equation	Init (u)	Init (ut)	Description
netflow	netflowt-(inflow+outflow)/(2*Ttot)	0	0	



# 7. Integration Coupling Variables

7.1. Geom1

7.1.1. Source Boundary: 2

Name	Value
Variable name	inflow
Expression	2*pi*r*v
Order	4
Global	Yes

## 7.1.2. Source Boundary: 3

Name	Value
Variable name	outflow
Expression	2*pi*r*v
Order	4
Global	Yes

### 7.1.3. Source Subdomain: 1

Name	Value
Variable name	Vol
Expression	2*pi*r
Order	4
Global	Yes

## 8. Functions

Function	Expression	Derivatives	Complex output
gauss(x,sigma)	1/(sigma*sqrt(2*pi))*exp(- x^2/(2*sigma^2))	d(1/(sigma*sqrt(2*pi))*exp(- x^2/(2*sigma^2)),x), d(1/(sigma*sqrt(2*pi))*exp(- x^2/(2*sigma^2)),sigma)	false



# 9. Solver Settings

Solve using a script: off

Analysis type	Transient
Auto select solver	On
Solver	Time dependent
Solution form	Automatic
Symmetric	Auto
Adaptive mesh refinement	Off
Optimization/Sensitivity	Off
Plot while solving	Off

# 9.1. Direct (PARDISO)

Solver type: Linear system solver

Parameter	Value
Preordering algorithm	Nested dissection
Row preordering	On
Bunch-Kaufmann	Off
Pivoting perturbation	1.0E-8
Relative tolerance	1.0E-6
Factor in error estimate	400.0
Check tolerances	Off

## 9.2. Time Stepping

Parameter	Value
Times	range(0,0.01,1.5)
Relative tolerance	0.01
Absolute tolerance	1e-3
Times to store in output	Specified times
Time steps taken by solver	Strict
Maximum BDF order	2
Singular mass matrix	Maybe
Consistent initialization of DAE systems	Backward Euler
Error estimation strategy	Exclude algebraic
Allow complex numbers	Off



# 9.3. Advanced

Parameter	Value
Constraint handling method	Elimination
Null-space function	Automatic
Automatic assembly block size	On
Assembly block size	1000
Use Hermitian transpose of constraint matrix and in symmetry detection	Off
Use complex functions with real input	Off
Stop if error due to undefined operation	On
Store solution on file	Off
Type of scaling	Automatic
Manual scaling	
Row equilibration	On
Manual control of reassembly	Off
Load constant	On
Constraint constant	On
Mass constant	On
Damping (mass) constant	On
Jacobian constant	On
Constraint Jacobian constant	On

## **10.** Postprocessing





### 11. Variables

### 11.1. Point 11.1.1. Point 1-2

Name	Description	Unit	Expression
RFR_axi	Reaction force R-dir.	Ν	
RFZ_axi	Reaction force Z-dir.	Ν	
FRg_axi	Point load in global R dir.	Ν	
FZg_axi	Point load in global Z dir.	Ν	
disp_axi	Total displacement	М	
uaxi_axi	R-displacement	m	
uaxiR_axi	R derivative of R-displacement	1	
uaxiZ_axi	Z derivative of R displacement	1	
uaxi_t_axi	R-velocity	m/s	
uaxi_tt_axi	R-acceleration	m/s^2	
rinit_ale	r coordinate initial value	m	R
zinit_ale	z coordinate initial value	m	Ζ

### 11.1.2. Point 3-6

Name	Description	Unit	Expression
RFR_axi	Reaction force R-dir.	Ν	if(R>0,2 * reacf(uor) * pi/R,0)
RFZ_axi	Reaction force Z-dir.	Ν	2 * reacf(w) * pi
FRg_axi	Point load in global R dir.	Ν	0
FZg_axi	Point load in global Z dir.	Ν	0
disp_axi	Total displacement	m	<pre>sqrt(real(uaxi_axi)^2+real(w)^2)</pre>
uaxi_axi	R-displacement	m	uor * R
uaxiR_axi	R derivative of R-displacement	1	uorR * R+uor
uaxiZ_axi	Z derivative of R displacement	1	uorZ * R
uaxi_t_axi	R-velocity	m/s	uort * R
uaxi_tt_axi	R-acceleration	m/s^2	uortt * R
rinit_ale	r coordinate initial value	m	R
zinit_ale	z coordinate initial value	m	Z



# 11.2. Boundary

## 11.2.1. Boundary 1-3

Name	Description	Unit	Expression
RFR_axi	Reaction force R-dir.	Ν	
RFZ_axi	Reaction force Z-dir.	Ν	
FRg_axi	Edge load in global R- dir.	N/m^2	
FZg_axi	Edge load in global Z- dir.	N/m^2	
disp_axi	Total displacement	m	
uaxi_axi	R-displacement	m	
uaxiR_axi	R derivative of R- displacement	1	
uaxiZ_axi	Z derivative of R displacement	1	
uaxi_t_axi	R-velocity	m/s	
uaxi_tt_axi	R-acceleration	m/s^2	
TaR_axi	Surface traction (force/area) in R dir.	Ра	
TaZ_axi	Surface traction (force/area) in Z dir.	Ра	
rinit_ale	r coordinate initial value	m	R
zinit_ale	z coordinate initial value	m	Ζ
K_r_chns	Viscous force per area, r component	Ра	eta_chns * (2 * nr_chns * ur+nz_chns * (uz+vr))
T_r_chns	Total force per area, r component	Ра	-nr_chns * p+2 * nr_chns * eta_chns * ur+nz_chns * eta_chns * (uz+vr)
K_z_chns	Viscous force per area, z component	Ра	eta_chns * (nr_chns * (vr+uz)+2 * nz_chns * vz)
T_z_chns	Total force per area, z component	Ра	-nz_chns * p+nr_chns * eta_chns * (vr+uz)+2 * nz_chns * eta_chns * vz

## 11.2.2. Boundary 4

Name	Description	Unit	Expression
RFR_axi	Reaction force R-dir.	Ν	if(R>0,2 * reacf(uor) * pi/R,0)
RFZ_axi	Reaction force Z-dir.	Ν	2 * reacf(w) * pi
FRg_axi	Edge load in global	N/m^2	0



	R-dir.		
FZg_axi	Edge load in global Z-dir.	N/m^2	0
disp_axi	Total displacement	М	sqrt(real(uaxi_axi)^2+real(w)^2)
uaxi_axi	R-displacement	М	uor * R
uaxiR_axi	R derivative of R- displacement	1	uorR * R+uor
uaxiZ_axi	Z derivative of R displacement	1	uorZ * R
uaxi_t_axi	R-velocity	m/s	uort * R
uaxi_tt_axi	R-acceleration	m/s^2	uortt * R
TaR_axi	Surface traction (force/area) in R dir.	Ра	sR_axi * nR_axi+sRZ_axi * nZ_axi
TaZ_axi	Surface traction (force/area) in Z dir.	Ра	sRZ_axi * nR_axi+sZ_axi * nZ_axi
rinit_ale	r coordinate initial value	М	R
zinit_ale	z coordinate initial value	М	Z
K_r_chns	Viscous force per area, r component	Ра	eta_chns * (2 * nr_chns * ur+nz_chns * (uz+vr))
T_r_chns	Total force per area, r component	Ра	-nr_chns * p+2 * nr_chns * eta_chns * ur+nz_chns * eta_chns * (uz+vr)
K_z_chns	Viscous force per area, z component	Ра	eta_chns * (nr_chns * (vr+uz)+2 * nz_chns * vz)
T_z_chns	Total force per area, z component	Ра	-nz_chns * p+nr_chns * eta_chns * (vr+uz)+2 * nz_chns * eta_chns * vz

# 11.2.3. Boundary 5-6

Name	Description	Unit	Expression
RFR_axi	Reaction force R-dir.	N	if(R>0,2 * reacf(uor) * pi/R,0)
RFZ_axi	Reaction force Z-dir.	Ν	2 * reacf(w) * pi
FRg_axi	Edge load in global R-dir.	N/m^2	0
FZg_axi	Edge load in global Z-dir.	N/m^2	0
disp_axi	Total displacement	m	<pre>sqrt(real(uaxi_axi)^2+real(w)^2)</pre>
uaxi_axi	R-displacement	m	uor * R
uaxiR_axi	R derivative of R-displacement	1	uorR * R+uor
uaxiZ_axi	Z derivative of R displacement	1	uorZ * R



uaxi_t_axi	R-velocity	m/s	uort * R
uaxi_tt_axi	R-acceleration	m/s^2	uortt * R
TaR_axi	Surface traction (force/area) in R dir.	Ра	sR_axi * nR_axi+sRZ_axi * nZ_axi
TaZ_axi	Surface traction (force/area) in Z dir.	Ра	sRZ_axi * nR_axi+sZ_axi * nZ_axi
rinit_ale	r coordinate initial value	m	R
zinit_ale	z coordinate initial value	m	Ζ
K_r_chns	Viscous force per area, r component	Ра	
T_r_chns	Total force per area, r component	Ра	
K_z_chns	Viscous force per area, z component	Pa	
T_z_chns	Total force per area, z component	Ра	

# 11.2.4. Boundary 7

Name	Description	Unit	Expression
RFR_axi	Reaction force R-dir.	Ν	if(R>0,2 * reacf(uor) * pi/R,0)
RFZ_axi	Reaction force Z-dir.	Ν	2 * reacf(w) * pi
FRg_axi	Edge load in global R-dir.	N/m^2	FR_axi
FZg_axi	Edge load in global Z-dir.	N/m^2	0
disp_axi	Total displacement	m	<pre>sqrt(real(uaxi_axi)^2+real(w)^2)</pre>
uaxi_axi	R-displacement	m	uor * R
uaxiR_axi	R derivative of R-displacement	1	uorR * R+uor
uaxiZ_axi	Z derivative of R displacement	1	uorZ * R
uaxi_t_axi	R-velocity	m/s	uort * R
uaxi_tt_axi	R-acceleration	m/s^2	uortt * R
TaR_axi	Surface traction (force/area) in R dir.	Ра	sR_axi * nR_axi+sRZ_axi * nZ_axi
TaZ_axi	Surface traction (force/area) in Z dir.	Ра	sRZ_axi * nR_axi+sZ_axi * nZ_axi
rinit_ale	r coordinate initial value	m	R
zinit_ale	z coordinate initial value	m	Ζ
K_r_chns	Viscous force per area, r component	Ра	
T_r_chns	Total force per area, r	Pa	


	component		
K_z_chns	Viscous force per area, z component	Ра	
T_z_chns	Total force per area, z component	Ра	

## 11.3. Subdomain

## 11.3.1. Subdomain 1

Name	Description	Unit	Expression
RFR_axi	Reaction force R- dir.	Ν	
RFZ_axi	Reaction force Z- dir.	N	
FRg_axi	Body load in global R-dir.	N/m^3	
FZg_axi	Body load in global Z-dir.	N/m^3	
disp_axi	Total displacement	М	
uaxi_axi	R-displacement	М	
uaxiR_axi	R derivative of R- displacement	1	
uaxiZ_axi	Z derivative of R displacement	1	
uaxi_t_axi	R-velocity	m/s	
uaxi_tt_axi	R-acceleration	m/s^2	
sR_axi	sR normal stress global sys.	Ра	
sZ_axi	sZ normal stress global sys.	Ра	
sPHI_axi	sPHI normal stress	Ра	
sRZ_axi	sRZ shear stress global sys.	Ра	
eR_axi	eR normal strain global sys.	1	
eZ_axi	eZ normal strain global sys.	1	
ePHI_axi	ePHI normal strain	1	
eRZ_axi	eRZ shear strain	1	



	global sys.		
sr_t_axi	Time der. of normal stress global sys. (sR)	Pa/s	
sz_t_axi	Time der. of normal stress global sys. (sZ)	Pa/s	
sphi_t_axi	Time der. of normal stress (sPHI)	Pa/s	
srz_t_axi	Time der. of shear stress global sys. (sRZ)	Pa/s	
er_t_axi	eR_t normal velocity strain global sys.	1/s	
ez_t_axi	eZ_t normal velocity strain global sys.	1/s	
ephi_t_axi	ePHI_t normal velocity strain	1/s	
erz_t_axi	eRPHI_t shear velocity strain global sys.	1/s	
mises_axi	von Mises stress	Pa	
Ws_axi	Strain energy density	J/m^3	
evol_axi	Volumetric strain	1	
tresca_axi	Tresca stress	Pa	
rinit_ale	r coordinate initial value	m	R
zinit_ale	z coordinate initial value	m	Z
dr_ale	r-displacement	m	r-R
dz_ale	z-displacement	m	z-Z
U_chns	Velocity field	m/s	sqrt(u^2+v^2)
V_chns	Vorticity	1/s	uz-vr
divU_chns	Divergence of velocity field	1/s	ur+vz+u/r
sr_chns	Shear rate	1/s	sqrt(0.5 * (4 * ur <sup>2</sup> +2 * (uz+vr) <sup>2</sup> +4 * vz <sup>2</sup> +4 * u <sup>2</sup> /(r+eps) <sup>2</sup> )+eps)



cellRe_chns	Cell Reynolds number	1	rho_chns * U_chns * h_ale/eta_chns
res_u_chns	Equation residual for u	Pa	r * (rho_chns * (ut+u * ur+v * uz)+pr- F_r_chns)+2 * eta_chns * (u/r-ur)- eta_chns * r * (2 * urr+uzz+vrz)
res_v_chns	Equation residual for v	Ра	r * (rho_chns * (vt+u * vr+v * vz)+pz- F_z_chns)-eta_chns * (r * (vrr+uzr)+2 * r * vzz+uz+vr)
beta_r_chns	Convective field, r component	Pa*s	r * rho_chns * u
beta_z_chns	Convective field, z component	Pa*s	r * rho_chns * v
Dm_chns	Mean diffusion coefficient	kg/s	r * eta_chns
da_chns	Total time scale factor	kg/m^2	r * rho_chns
taum_chns	GLS time-scale	m^3*s/kg	nojac(1/max(2 * rho_chns * sqrt(emetric_ale(u-rt,v-zt)),48 * eta_chns/h_ale^2))
tauc_chns	GLS time-scale	m^2/s	0.5 * nojac(if((u-rt)^2+(v-zt)^2<=""" td="">
res_p_chns	Equation residual for p	kg/(m^2*s)	rho_chns * r * divU_chns

# 11.3.2. Subdomain 2

Name	Description	Unit	Expression
RFR_axi	Reaction force R-dir.	Ν	if(R>0,2 * reacf(uor) * pi/R,0)
RFZ_axi	Reaction force Z-dir.	Ν	2 * reacf(w) * pi
FRg_axi	Body load in global R-dir.	N/m^3	0
FZg_axi	Body load in global Z-dir.	N/m^3	0
disp_axi	Total displacement	М	sqrt(real(uaxi_axi)^2+real(w)^2)
uaxi_axi	R-displacement	М	uor * R
uaxiR_axi	R derivative of R-displacement	1	uorR * R+uor
uaxiZ_axi	Z derivative of	1	uorZ * R



	R displacement		
uaxi_t_axi	R-velocity	m/s	uort * R
uaxi_tt_axi	R-acceleration	m/s^2	uortt * R
sR_axi	sR normal stress global sys.	Pa	E_axi * ((1-nu_axi) * eR_axi+nu_axi * ePHI_axi+nu_axi * eZ_axi)/((1+nu_axi) * (1- 2 * nu_axi))
sZ_axi	sZ normal stress global sys.	Pa	E_axi * (nu_axi * eR_axi+nu_axi * ePHI_axi+(1-nu_axi) * eZ_axi)/((1+nu_axi) * (1-2 * nu_axi))
sPHI_axi	sPHI normal stress	Ра	E_axi * (nu_axi * eR_axi+(1-nu_axi) * ePHI_axi+nu_axi * eZ_axi)/((1+nu_axi) * (1- 2 * nu_axi))
sRZ_axi	sRZ shear stress global sys.	Ра	E_axi * eRZ_axi/(1+nu_axi)
eR_axi	eR normal strain global sys.	1	uorR * R+uor
eZ_axi	eZ normal strain global sys.	1	wZ
ePHI_axi	ePHI normal strain	1	uor
eRZ_axi	eRZ shear strain global sys.	1	0.5 * (uorZ * R+wR)
sr_t_axi	Time der. of normal stress global sys. (sR)	Pa/s	E_axi * ((1-nu_axi) * er_t_axi+nu_axi * ephi_t_axi+nu_axi * ez_t_axi)/((1+nu_axi) * (1-2 * nu_axi))
sz_t_axi	Time der. of normal stress global sys. (sZ)	Pa/s	E_axi * (nu_axi * er_t_axi+nu_axi * ephi_t_axi+(1-nu_axi) * ez_t_axi)/((1+nu_axi) * (1-2 * nu_axi))
sphi_t_axi	Time der. of normal stress (sPHI)	Pa/s	E_axi * (nu_axi * er_t_axi+(1-nu_axi) * ephi_t_axi+nu_axi * ez_t_axi)/((1+nu_axi) * (1-2 * nu_axi))
srz_t_axi	Time der. of shear stress global sys. (sRZ)	Pa/s	E_axi * erz_t_axi/(1+nu_axi)
er_t_axi	eR_t normal velocity strain global sys.	1/s	uorRt * R+uort
ez_t_axi	eZ_t normal	1/s	wZt



	velocity strain global sys.		
ephi_t_axi	ePHI_t normal velocity strain	1/s	uort
erz_t_axi	eRPHI_t shear velocity strain global sys.	1/s	0.5 * (uorZt * R+wRt)
mises_axi	von Mises stress	Pa	sqrt(sR_axi^2+sPHI_axi^2+sZ_axi^2-sR_axi * sPHI_axi-sPHI_axi * sZ_axi-sR_axi * sZ_axi+3 * sRZ_axi^2)
Ws_axi	Strain energy density	J/m^3	0.5 * (eR_axi * sR_axi+ePHI_axi * sPHI_axi+eZ_axi * sZ_axi+2 * eRZ_axi * sRZ_axi)
evol_axi	Volumetric strain	1	eR_axi+ePHI_axi+eZ_axi
tresca_axi	Tresca stress	Ра	max(max(abs(s1_axi-s2_axi),abs(s2_axi- s3_axi)),abs(s1_axi-s3_axi))
rinit_ale	r coordinate initial value	М	R
zinit_ale	z coordinate initial value	М	Z
dr_ale	r-displacement	М	r-R
dz_ale	z-displacement	М	z-Z
U_chns	Velocity field	m/s	
V_chns	Vorticity	1/s	
divU_chns	Divergence of velocity field	1/s	
sr_chns	Shear rate	1/s	
cellRe_chns	Cell Reynolds number	1	
res_u_chns	Equation residual for u	Ра	
res_v_chns	Equation residual for v	Ра	
beta_r_chns	Convective field, r component	Pa*s	
beta_z_chns	Convective field, z component	Pa*s	
Dm_chns	Mean diffusion	kg/s	



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	coefficient		
da_chns	Total time scale factor	kg/m^2	
taum_chns	GLS time-scale	m^3*s/kg	
tauc_chns	GLS time-scale	m^2/s	
res_p_chns	Equation residual for p	kg/(m^2*s)	



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### ABSTRACT

### NOVEL PULSATILE CARDIAC ASSIST PUMP

by

#### LAKSHMI MOHANADAS

### May 2015

Advisor: Dr. Gregory W Auner

Major: Biomedical Engineering

Degree: Master of Science

The project involve the research and development of a pulsatile, complex or continuous flow in biological and non-biological systems implantable heart assist pump. Specifically as a 20% cardiac assist for persons from congestive heart failure and other cardiac abnormalities. The pulsatile cardiac assist pump would provide upto 20% of the blood pumping process from the venous supply to the arterial supply. Current pumps are largely complete bypass pumps or large volume pumps that produce significant long term blood cell damage resulting in thrombosis. Most are not pulsatile which offers a significant physiological advantage. The pump under development is designed to prevent thrombosis by utilizing a unique geometry and pumping actuation mechanism. As part of the research we first used COSMOL simulation to aid in the design and blood flow dynamics. From these results we have designed a working prototype that can be configured in a number of geometries or stages. This design utilizes biocompatible material, Polyethylene oxide (PEO), which minimized protein interaction with the interior pumping surface. Shape memory alloy



actuators compress the pumping chamber. Shape memory alloy actuators also actuate compression of the ingoing sphincter valve and outgoing sphincter valves. Pumping motion can be analyzed by accelerometers to provide optimized feedback and pump motion control. Zoned compression may allow optimal compression for blood flow. This type of pumping system biomimics actual heart compression and pulsation while the sphincter like valves minimizes thrombosis causing turbulent. A second actuation method may be employed utilizing pneumatic cuffs that inflate and compress the pump body and sphincter valves. The pump has a minimum of one hundred twenty mmHg pressure capabilities at fifty to one hundred and fifty beats per minute or in coordination with the compression and decompression rate of the heart as measured by blood pressure sensors or direct heart electro cardiac sensing. A cluster of pumps each independently controlled may be packaged for sequence or sequential actuation providing complex pumping and flow patterns or continuous pumping flow. Further the pumps may be independently actuated in a tandem configuration. As such the pump provides a broad field of use including but not limited to arterial to arterial pumping, drug delivery, physiological fluidic maintenance, intravenous delivery, pressure maintenance and drug manufacturing where low turbulence flow is required and any pulsatile, complex flow pattern or continuous flow pattern is required.



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